

Fickian and Non-Fickian Diffusion with Bimolecular Reactions

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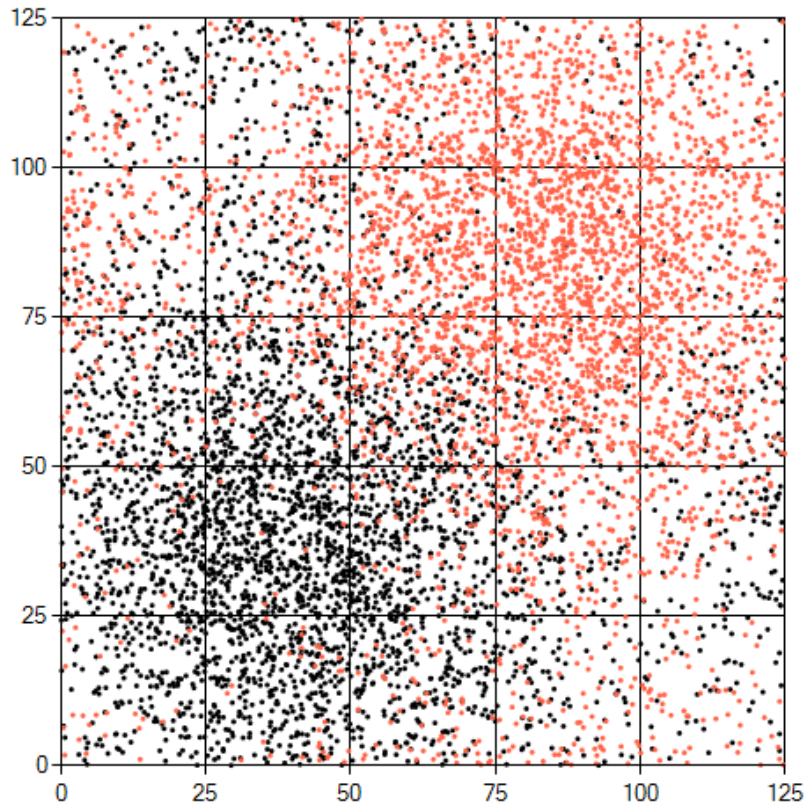


Rehovot, Israel

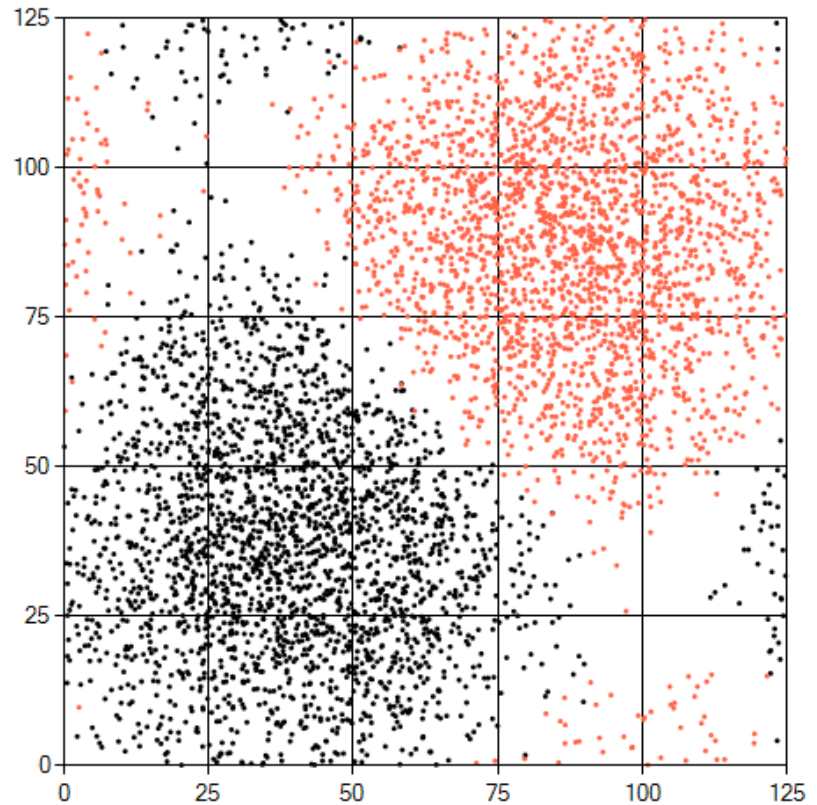
Reaction-Diffusion Phenomena

- Relevance: geochemical systems (precipitation/dissolution, CO_2), physics, biology (cells)
- Bimolecular reactions: $A + B \rightarrow C$
- Treatment via partial differential equation (PDE) and particle tracking (PT) approaches
(incorporation of effects of small-scale fluctuations!!!)
- Diffusion mechanism: Fickian, non-Fickian (“anomalous”)
- Reaction term:
PDE, Fickian: $\Gamma c_A c_B$, with Γ a reaction constant
PDE, non-Fickian: analytically intractable
- Particle Tracking: Continuous Time Random Walk (CTRW)
→ effectively quantifies anomalous transport and diffusion

Reactions: Averaging Effects



smaller R



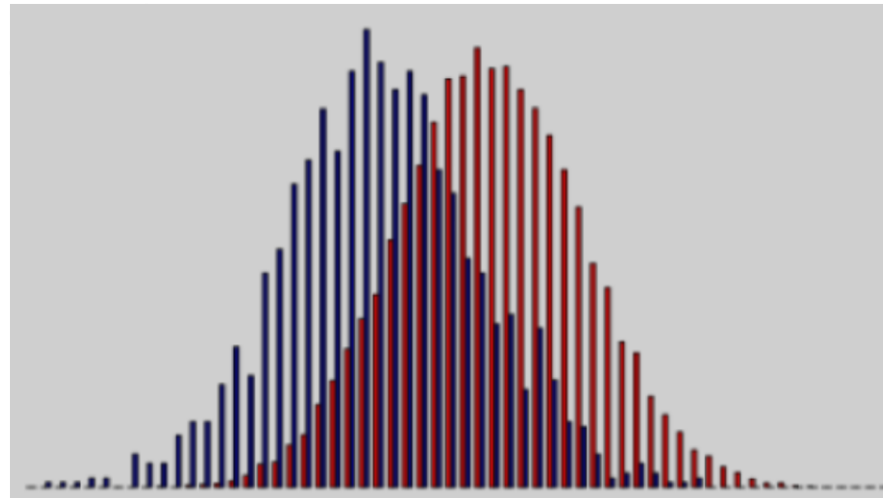
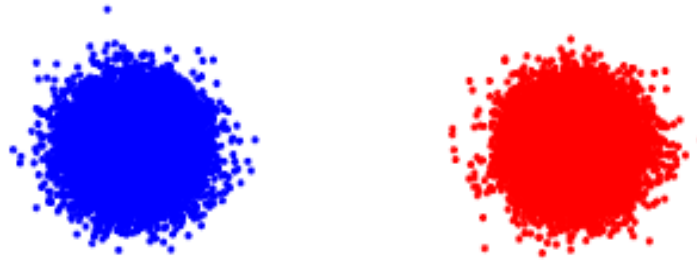
larger R

A and B diffuse, initially injected at separated points. Production of C (not shown) occurs when A , B are within a reaction radius R , which sets the small scale.

Small R enhances interpenetration of A , B .

Large R (= faster reaction rate) leads to a sharp reaction front
→ limiting mixing, but due to greater reaction

Question: For point injection of reactive species A and B , what are patterning dynamics of product $A + B \rightarrow C$?



- Concentration profiles for Fickian / non-Fickian diffusion?
- C may precipitate (immobile) or remain in solution (diffuse)

Modeling: CTRW Particle Tracking

- Particle tracking advantage: can study influence of small-scale fluctuations in species concentrations on reaction mixing and pattern formation (localized, pore-scale nature of reactions)
- Continuous Time Random Walk (CTRW): easily accounts for Fickian and non-Fickian diffusion
- $\mathbf{s}^{(N+1)} = \mathbf{s}^{(N)} + \boldsymbol{\zeta}^{(N)}, \quad t^{(N+1)} = t^{(N)} + \tau^{(N)}$

$\mathbf{s}^{(N)}, t^{(N)}$ denote location of a particle in space-time after N steps; spatial $\boldsymbol{\zeta}^{(N)}$ and temporal $\tau^{(N)}$ random increments assigned to particle transitions via a joint probability density $\psi(\mathbf{s}, t)$

Decoupled form: $\psi(\mathbf{s}, t) = p(\mathbf{s}) \psi(t)$ [independent pdf's]

Temporal pdf controls the character of the diffusion

Modeling Aspects

Spatial: normal distribution for $p(s)$, radially uniform angular component

Temporal:

Fickian diffusion: $\psi(t) = \lambda_t \exp(-\lambda_t t)$ [mean = $1/\lambda_t$]

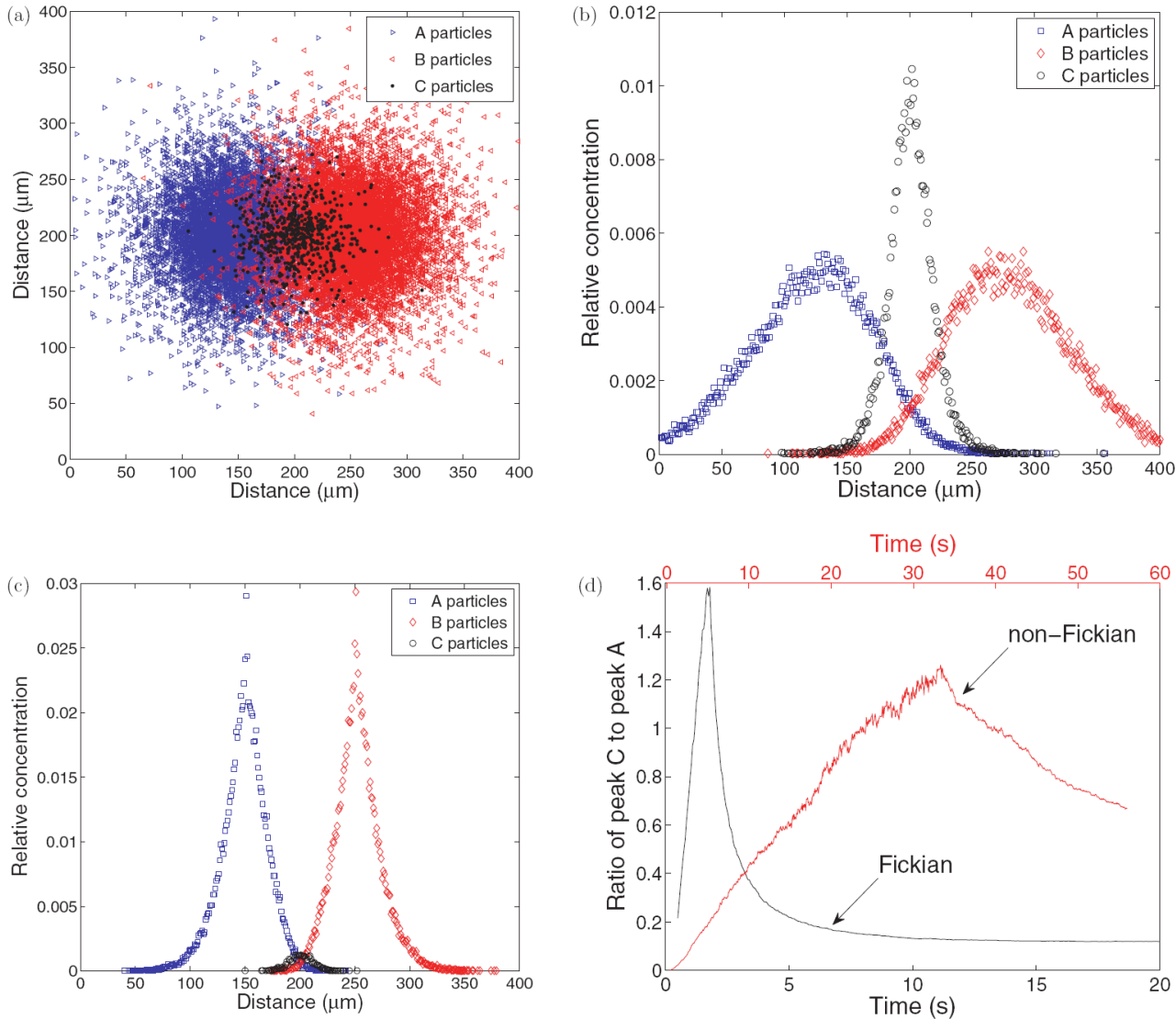
Non-Fickian diffusion, Truncated power law: $\psi(t) = \frac{n}{t_1} \exp(-t/t_2) / (1 + t/t_1)^{1+\beta}$

$0 < \beta < 2$, measure of the degree of anomaly; n normalization constant;

$\psi(t) \sim (t/t_1)^{-1-\beta}$ for $t_1 \ll t \ll t_2$; $\psi(t)$ decreases exponentially for $t \gg t_2$

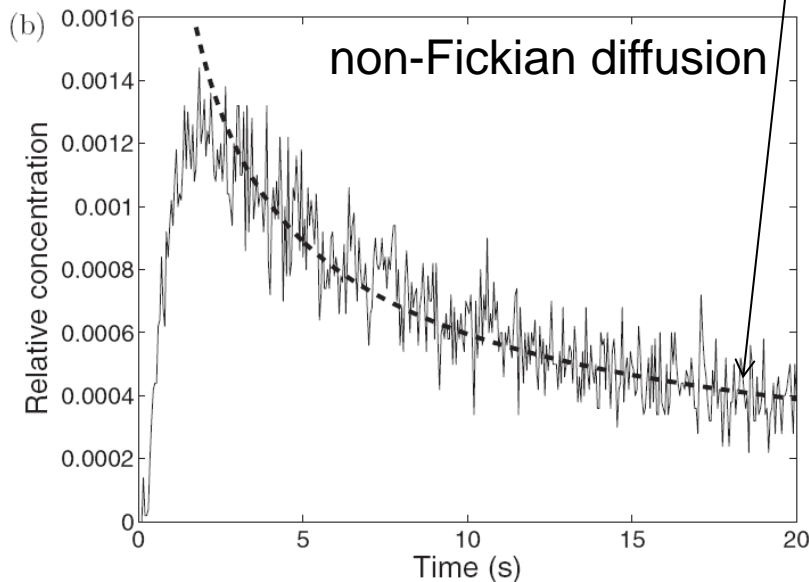
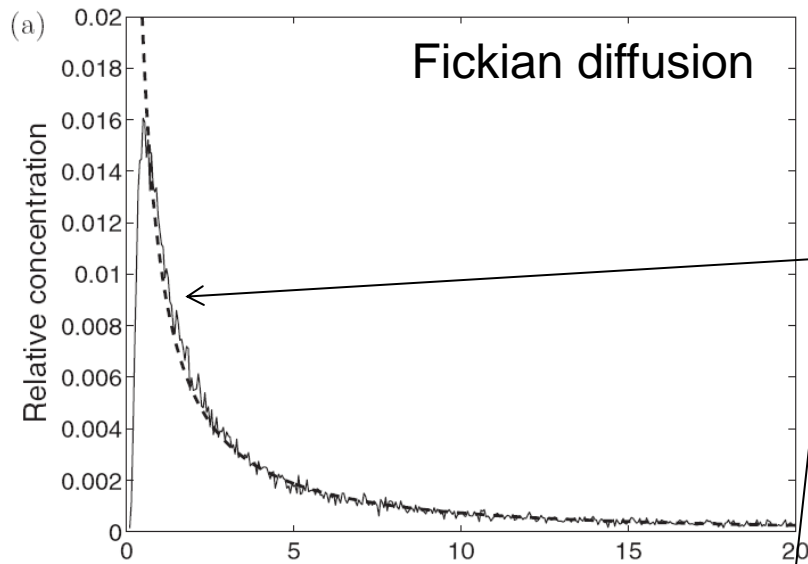
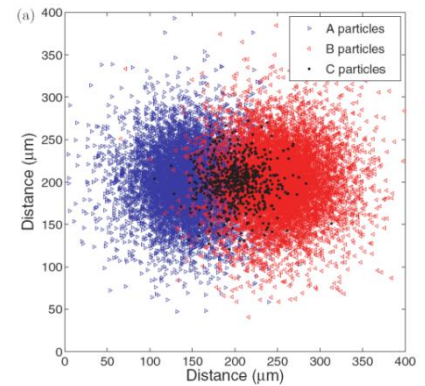
- Diffusion: $D = \varepsilon^2 / (4\delta t)$; with ε , δt = mean step length, transition time
- Choose $D = 10^{-9}$ m²/s (Fickian: normal $p(s)$, mean $\varepsilon = 10$ μ m, $\sigma = 1$)
- 50,000 particles each of A , B ; injection points separated by 100 μ m
- Non-Fickian: $\beta = 0.7$, $t_1 = \delta t$ (median transition step matched to Fickian), t_2 large
- Reaction radius: $R = 0.1$ μ m
- C particles immobile (in cases shown here)

Concentration Patterns and Profiles



- (a) Representative spatial A and B plume patterns, interacting to produce C ($T = 15$ s) for Fickian diffusion.
- (b),(c) Spatially integrated (over y axis) concentration profiles of A , B , and C particles, at $T = 2$ s, for (b) Fickian diffusion and (c) non-Fickian diffusion with $\beta = 0.7$.
- (d) Ratios of peaks of spatially integrated C profile to A profiles, over time, for Fickian diffusion and non-Fickian diffusion.

Rate of C Particle Production

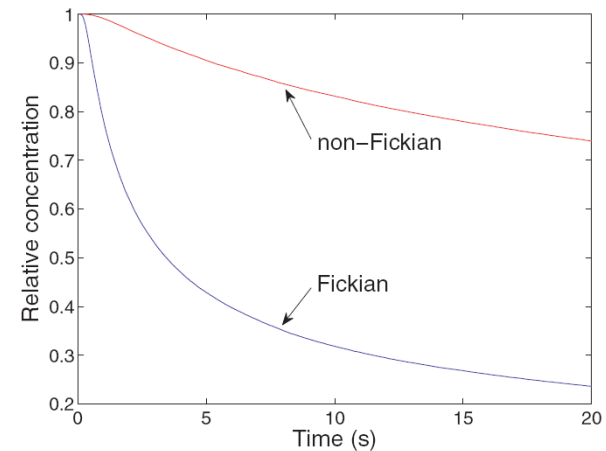


Dashed lines show fits of a stretched exponential function, $f(t) = \exp(-at^\gamma)$

Fickian: $a = 4.54$, $\gamma = 0.20$

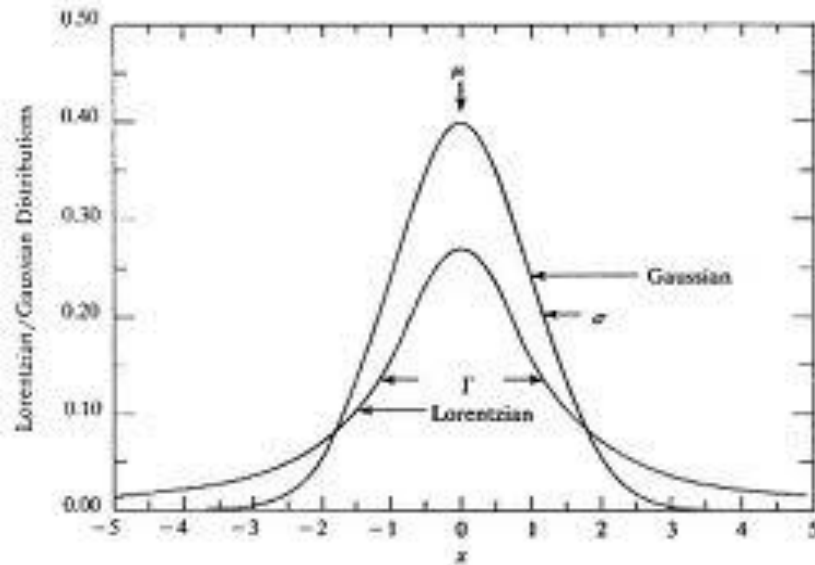
Non-Fickian): $a = 6.17$, $\gamma = 0.08$

[Note: y-axis scale larger for Fickian case]



Corresponding decrease in relative concentration of A (or B) particles over time, for Fickian and non-Fickian diffusion.

Gaussian and Lorentzian Characterization



Gaussian distribution: compact

Lorentzian (Cauchy) distribution:
heavy tailed (“broadening”)

*From previous figures, we expect C profiles to follow
a two-time regime evolution.*

Consider a weighted sum of a Gaussian and a Lorentzian:

$$a \exp[-|x - 200|^2 / (4dt^\alpha)] + b / [1 + c|x - 200|^2 / (dt^\alpha)]$$

where a , b , c , d , and α are fitting constants.

The relative weighting a/b is the key parameter of interest.

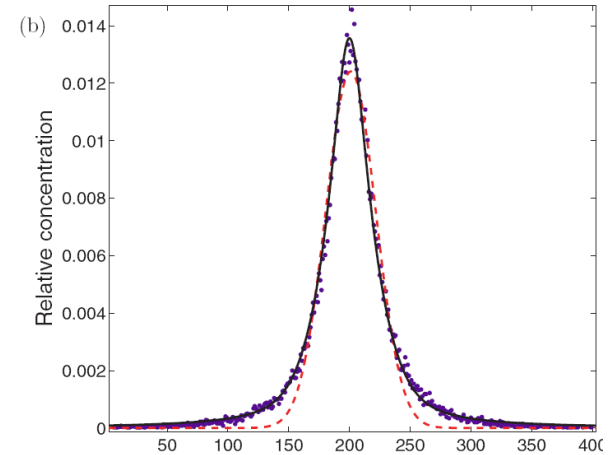
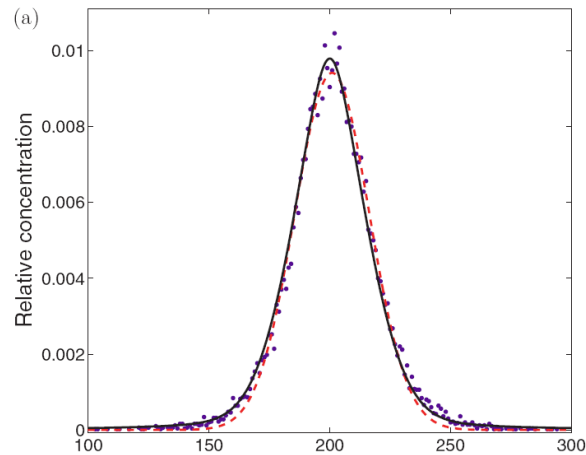
C Particle Concentration: Spatial Profiles

Spatially integrated (over y axis) concentration profiles of (immobile) C particles:

Fickian:

(a) $T = 2$ s

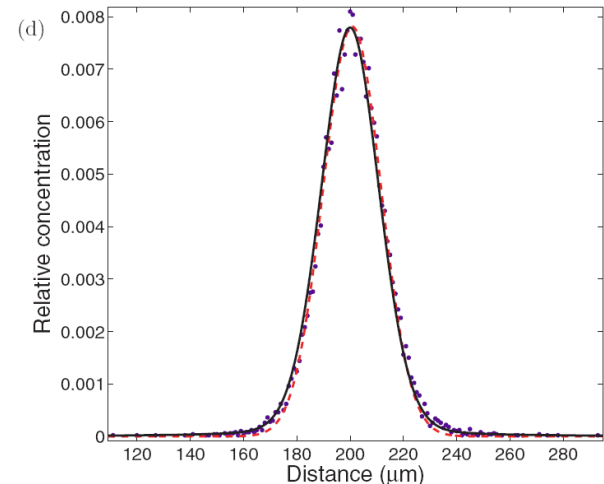
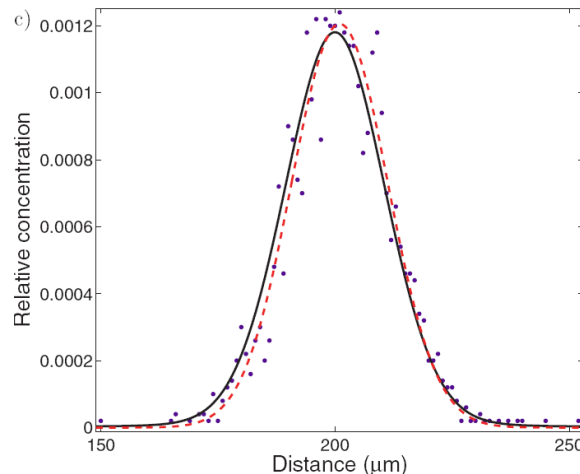
(b) $T = 15$ s



non-Fickian:

(c) $T = 2$ s

(d) $T = 15$ s



Profiles/curves are normalized by total number of C produced at the given time. Continuous curves show best fits of the weighted sum of **Gaussian** (weight a) and **Lorentzian** (weight b) distributions. Dashed lines (in red) are pure Gaussian fits.

Ratios of weights a/b (Gaussian/Lorentzian): (a) 2.1, (b) 0.3, (c) 12.8, and (d) 6.0.

Gaussian and Lorentzian Characterization

Fickian:

- Short times (a): profile reflects rapid compact growth in the reaction front region (= Gaussian)
- Longer times (b): C production builds up outside the reaction front region and the spatial extent of the profile spreads, with heavier tails
- \Rightarrow C profile for Fickian diffusion evolves, transiting from a compact Gaussian to a heavy tailed Lorentzian

non-Fickian:

- Over same time range, C profile remains Gaussian; a/b also decreases in time, but on a much larger time scale
- Difference in reaction patterns: a distinguishing feature of anomalous behavior (we do not detect $a/b < 1$ out to $T = 55$ s)

Experiment interpretation:

- Appearance of a Gaussian C profile does not prove that the diffusion process is Fickian!
- Can detect non-Fickian diffusion by comparing C profile dynamics to calculated expectations based on normal diffusion.

Additional Findings

- For mobile C particles (diffusing with same rules as A and B):
Fickian case: suppresses fluctuations and Gaussian behavior persists
non-Fickian case: C profiles have equal weights of Gaussian and Lorentzian components
- Times, distances show representative behaviors; larger and smaller (200 and 50 μm) distances between A and B injection points yield similar behaviors, with appropriate scaling
- Initial A and B vertical strip distribution yield the same C particle distribution behavior; the point or strip injection is not relevant
 \Rightarrow dynamics are basic phenomena which account for growth of concentration fluctuations, as the species numbers decline in the reaction front

Conclusions

- Mixing zone dynamics of a reaction product C during diffusion of two species (A and B) are examined, using a 2D particle tracking model for the reaction $A + B \rightarrow C$, allowing for both Fickian and non-Fickian transitions.
- Basic C pattern dynamics – temporal evolution of the spatial profile and the temporal C production – are similar for both modes of diffusion. But the distinctive time scale for the non-Fickian case is very much larger.
- For immobile C , the spatial profile pattern is a broadening (Gaussian) reaction front evolving to a concentration-fluctuation dominated (Lorentzian) shape. The temporal C production is fit by a stretched exponential.
- Analyzing experiments: appearance of Gaussian C profiles does not prove that the diffusion process is Fickian.

Origins of Anomalous Transport in Disordered Media: Structural and Dynamic Controls

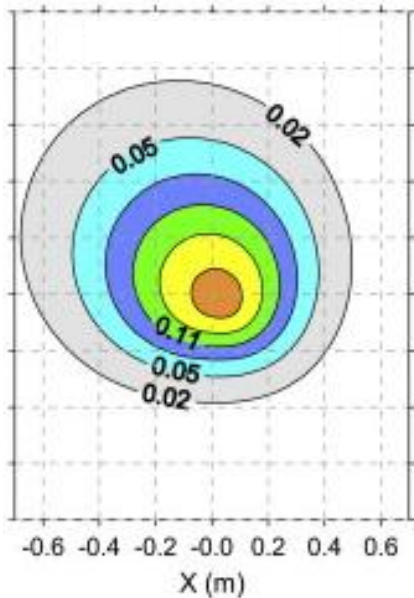
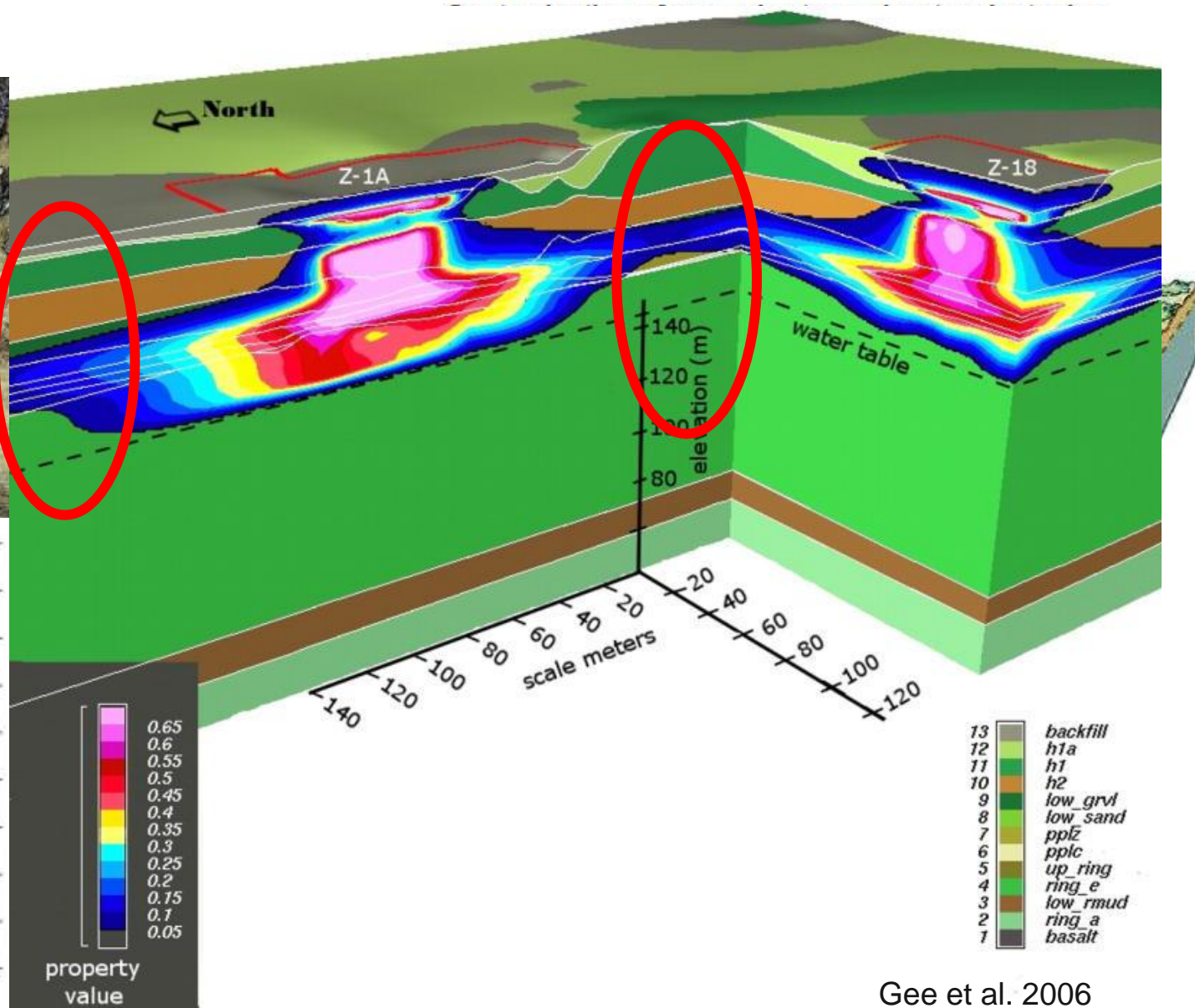
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Background



Meter scale uniform sand: non-Fickian behavior

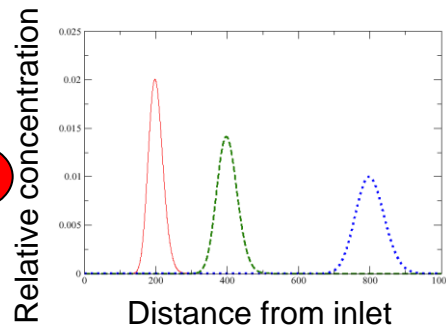
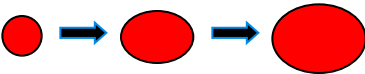
Even "homogeneous" systems are "anomalous"...



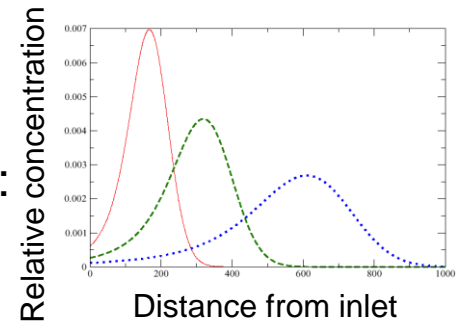
Flow direction →



"Expected"
Fickian:



"Actual"
non-Fickian:



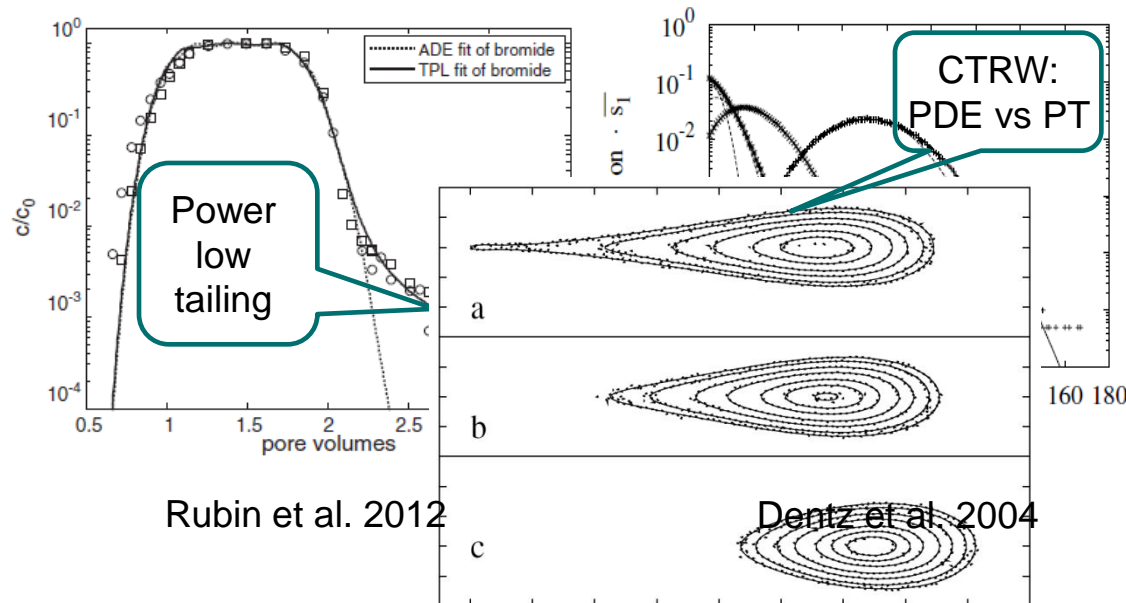
Probabilistic Approach: Continuous Time Random Walk

- ▶ Transport: sequence of particle transitions (in space and time)
- ▶ $\psi(s,t)$: Probability density function (pdf)
- ▶ Account for rare events: non-Fickian transport

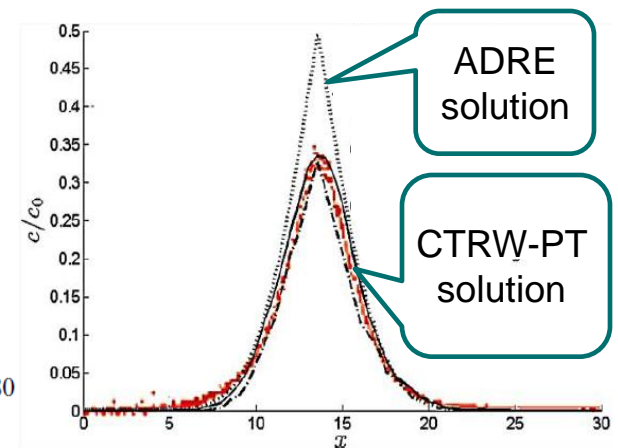
Generalized CTRW transport equation:

$$\tilde{M}(u) \equiv \bar{t} u \frac{\tilde{\psi}(u)}{1 - \tilde{\psi}(u)}; \quad u \tilde{c}(s, u) - C_0(s) = \tilde{M}(u) [v_\psi \cdot \nabla \tilde{c}(s, u) - D_\psi : \nabla \nabla \tilde{c}(s, u)]$$

Continuum approach: CTRW- PDE



Particle tracking: CTRW- PT



Edery et al. 2009

Transit time distribution $\psi(t)$: truncated power law (non-Fickian to Fickian evolution)

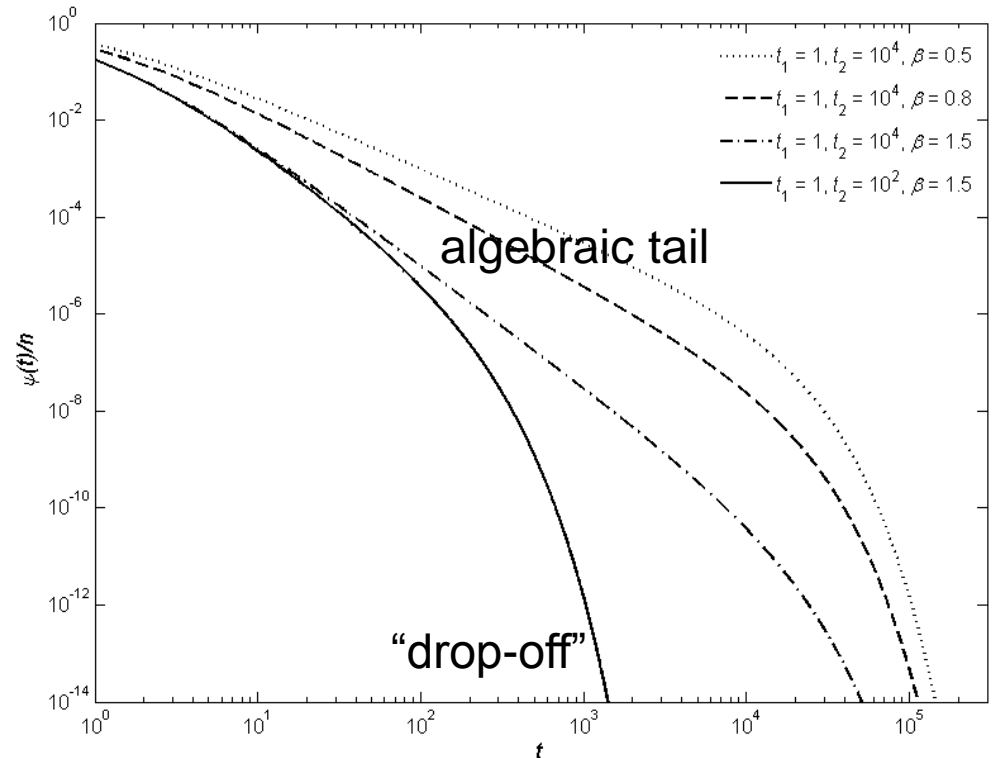
$$\psi(t) = \frac{n}{t_1} \frac{\exp(-\tau / \tau_2)}{(1 + \tau)^{1+\beta}}$$

$$\tau \equiv t/t_1, \quad \tau_2 \equiv t_2/t_1, \quad 0 < \beta < 2$$

n = normalization constant

$$\psi(t) \sim \tau^{-1-\beta} \quad \text{for } 1 \ll \tau \ll \tau_2$$

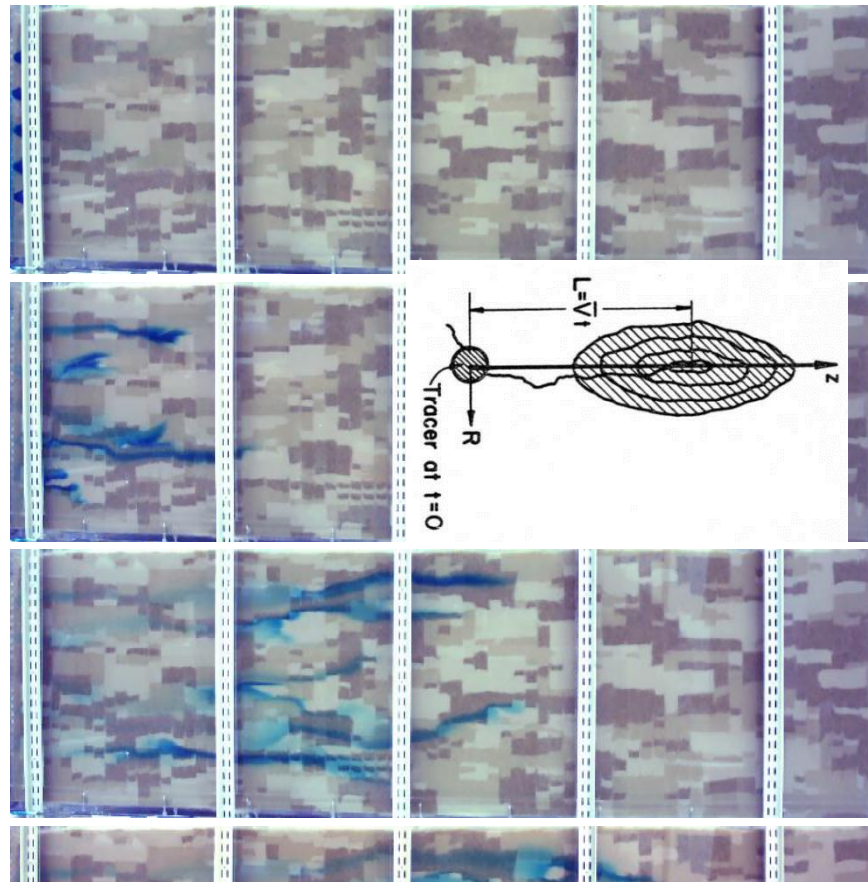
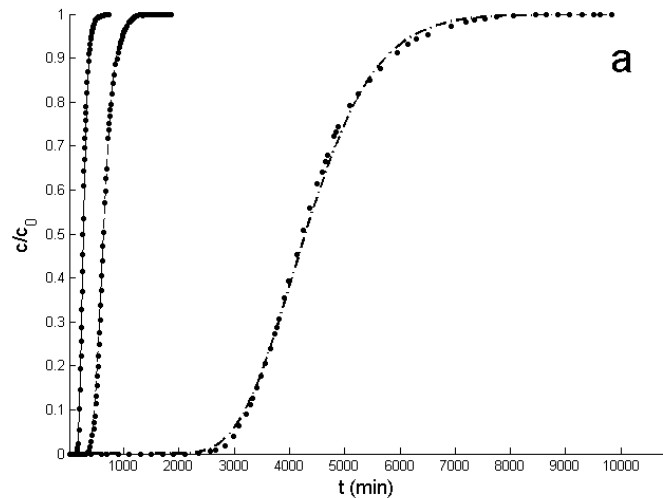
$\psi(t)$ decreases exponentially
for $\tau \gg \tau_2$



Note: (1) effect of cutoff time t_2 , (2) algebraic tail,
(3) drop-off (transition to Fickian)

Evidence for power law pdf: theoretical analyses, semi-analytical analyses of permeability/flow fields, numerical simulations of fluid flow / tracer transport, fits to measured tracer breakthrough curves

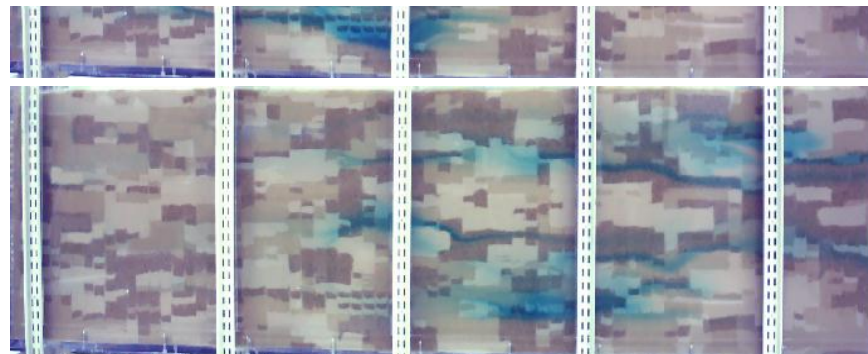
Non-Fickian transport in heterogeneous porous media



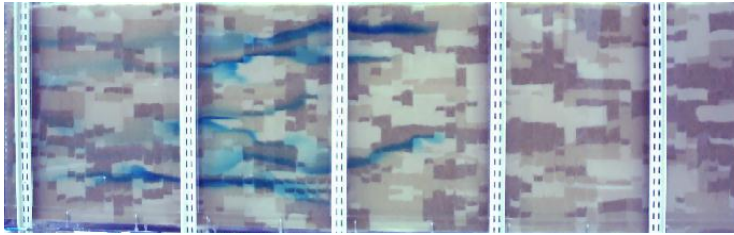
$$u\tilde{c}(\mathbf{s}, u) - c_o(\mathbf{s}) = -\tilde{M}(u) \left[\mathbf{v}_\psi \cdot \nabla \tilde{c}(\mathbf{s}, u) - \mathbf{D}_\psi : \nabla \nabla \tilde{c}(\mathbf{s}, u) \right]$$

$$\psi(t) = \frac{n}{t_1} \frac{\exp(-t/t_2)}{(1+t/t_1)^{1+\beta}}$$

Levy and Berkowitz, J Contam Hydrol 2003

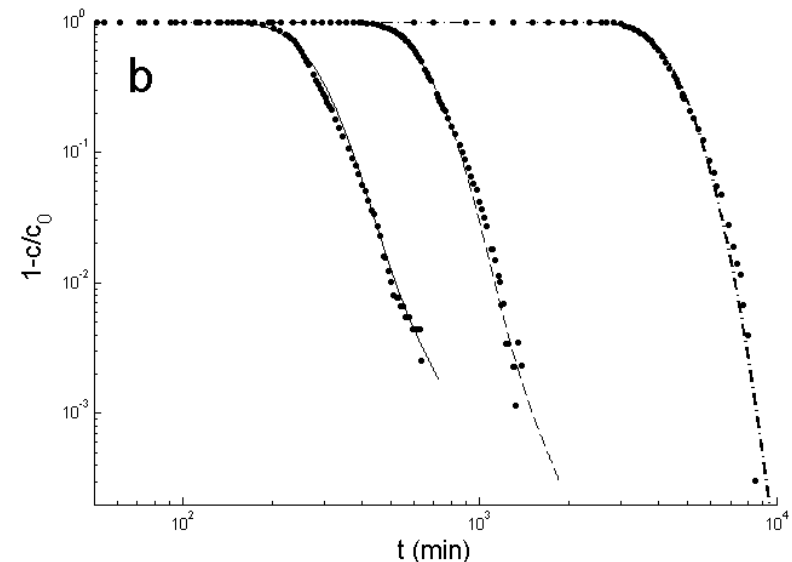
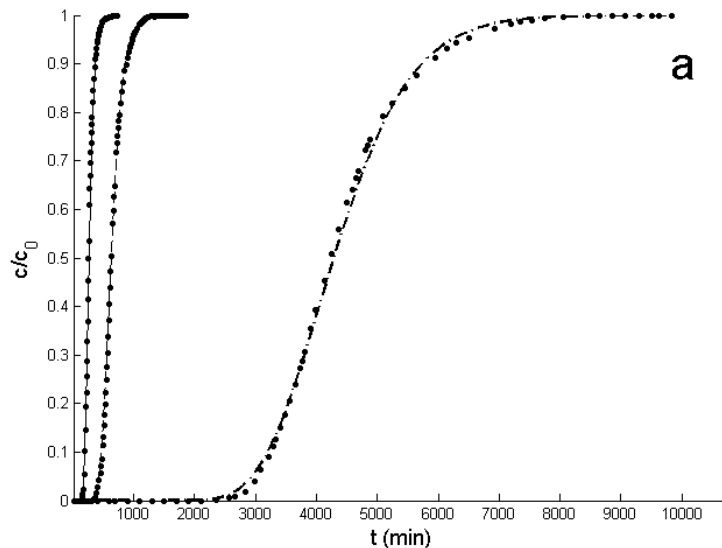


Plume Evolution: $\psi(t)$ sampled at different residence times



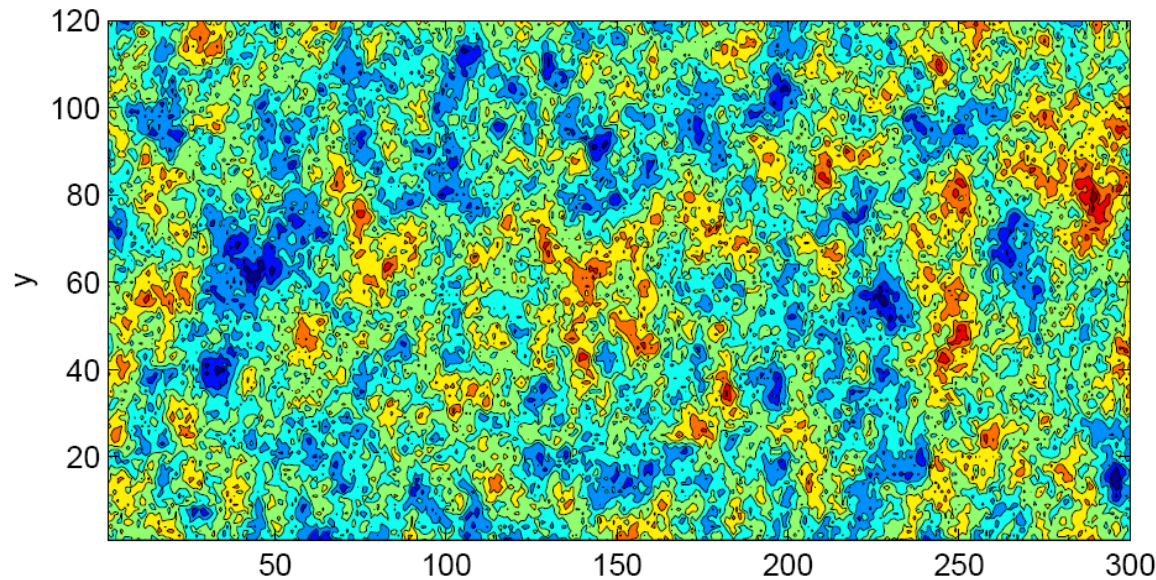
**Three experiments: flow rates
11, 74, 175 mL/min**

**Truncated power law $\psi(t)$:
constant exponent, parameter ratios for all curves**



[constant β , v_ψ/D_ψ , v/v_ψ , t_1 , t_2 ; with $t_1 = s/v_\psi$ and $s \approx 15\%$ average grain size]

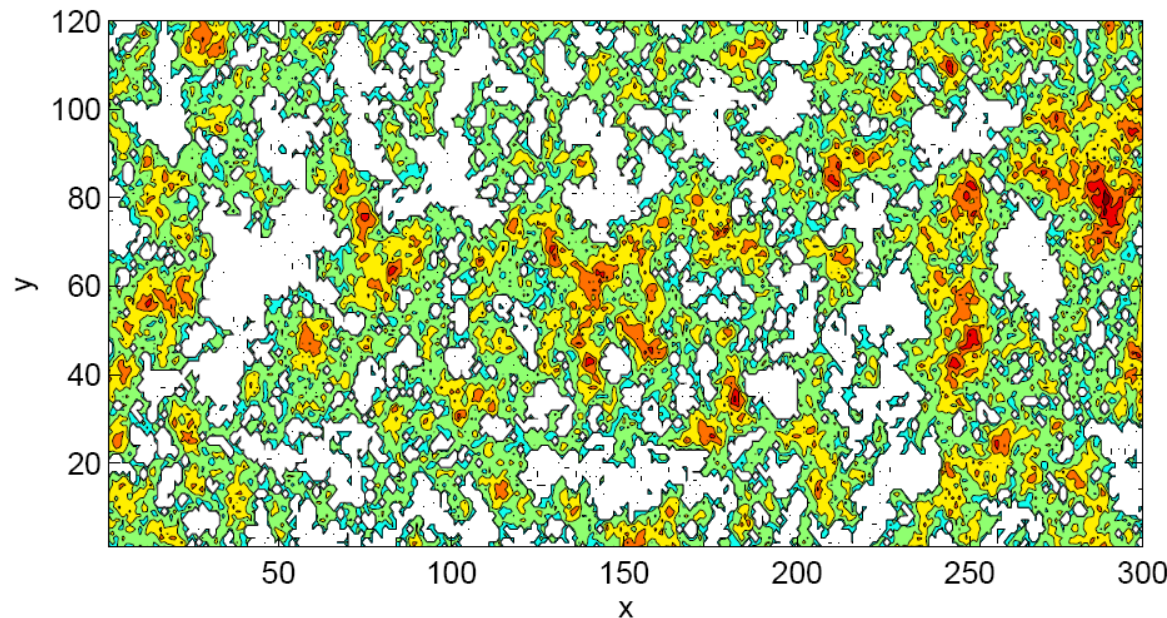
Natural Heterogeneity: Transport Patterns “Revisited”



Spatial map of full K field;
 $\ln(K)$ variance $\sigma^2=5$

Statistically homogeneous
and isotropic, multivariate
Gaussian field

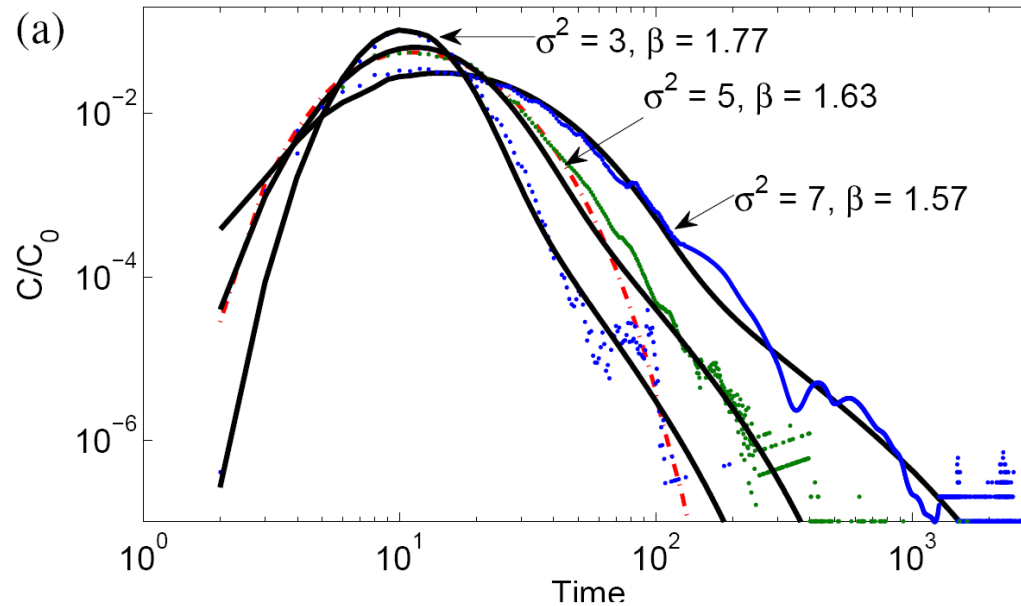
Color bar in $\ln(K)$ scale



As above; critical path
analysis (CPA); $\ln(K) < -0.63$



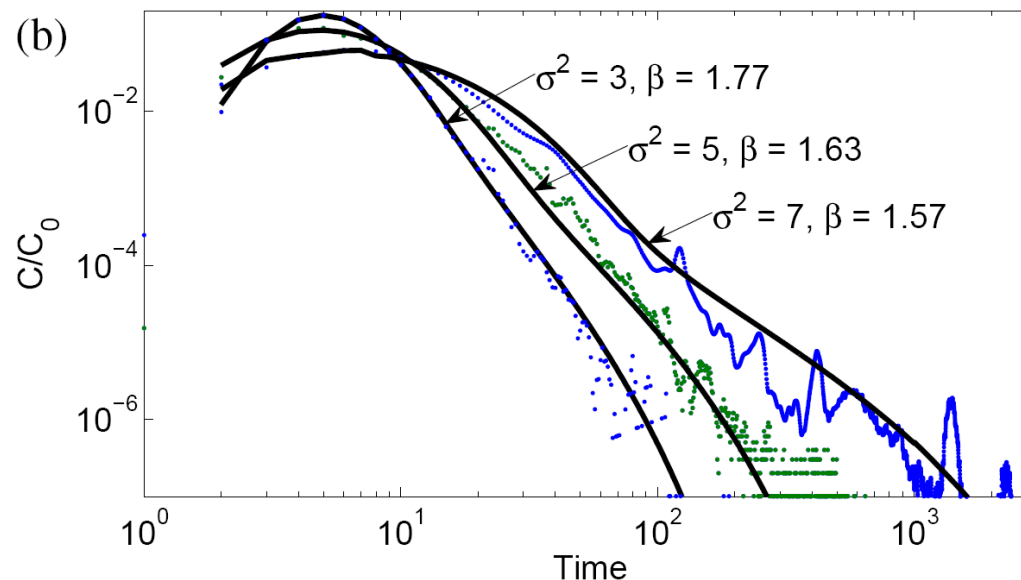
Transport Patterns “Revisited”: CTRW and ADE



Ensemble (100 realizations) breakthrough curves (points) for three $\ln(K)$ variances and corresponding CTRW fits.

(a) Domain boundary ($x=300$)

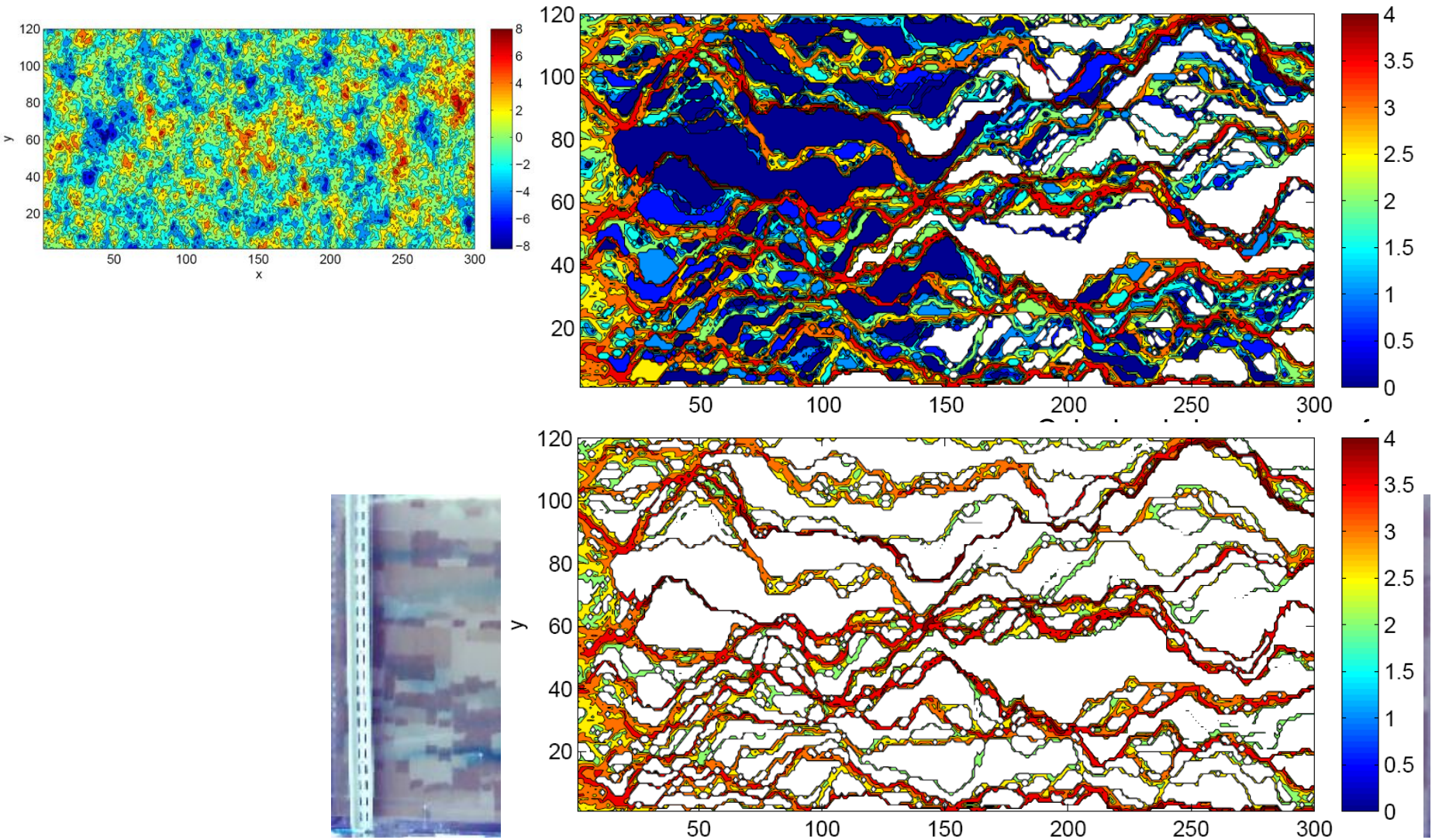
(b) Domain midpoint ($x=150$)



Also shown: ADE for $\sigma^2=5$ ($v=3.4$; but average fluid velocity = 5.6)

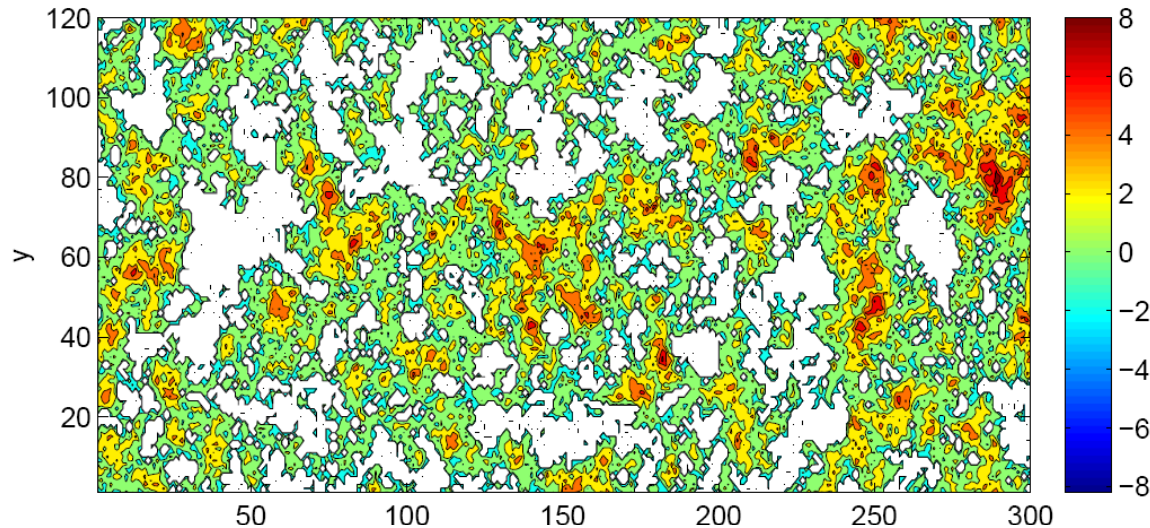
Oscillations in tails caused by formation of limited set of preferential channels, leading to variations in the distribution of small numbers of particles arriving at outlet.

Transport Patterns – Particle Interrogation of Domain



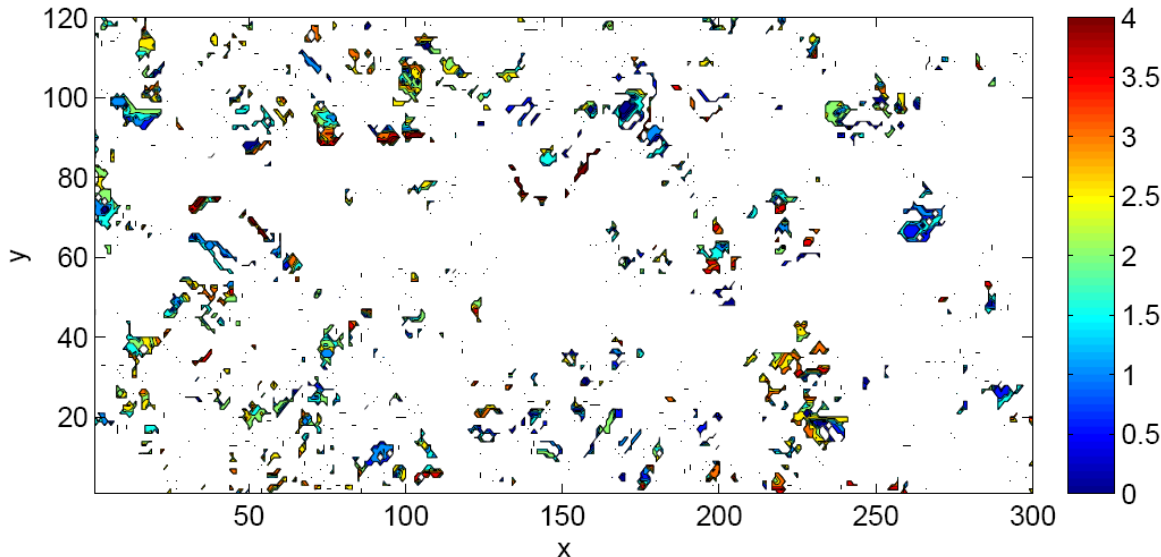
Upper: Particle paths (for $\sigma^2=5$). Note the formation of very limited set of preferential channels
Lower: Preferential particle paths (cells with visitation of >100 particles = 0.1% of all particles in domain)

Natural Heterogeneity: Critical Path Analysis / Percolation



Color bar in $\ln(K)$ scale

Note: *Inadequacy* of Critical Path Analysis (*based only on structure*)



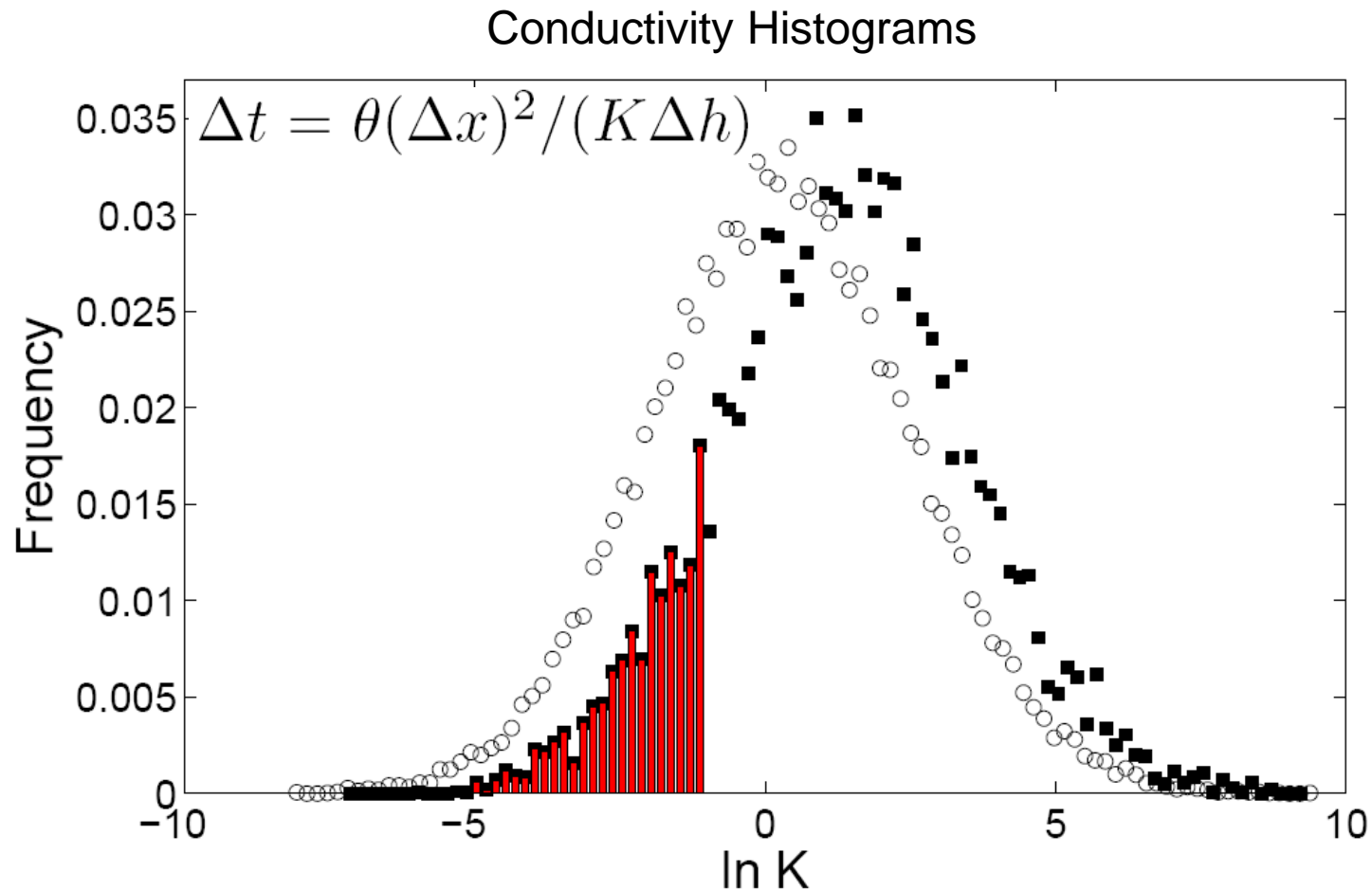
Cells with Low Conductivity Transitions (LCTs) of particles are a major, controlling factor!

Effect of K (or v) correlations: embedded in preferential paths, but they do not “predict” the low conductivity transitions.

Upper: Spatial map of full K field; $\ln(K)$ variance $\sigma^2=5$. Critical path analysis (CPA); $\ln(K) < -0.63$

Lower: Low conductivity transition cells (below CPA)

Natural Heterogeneity – Effective Conductivities

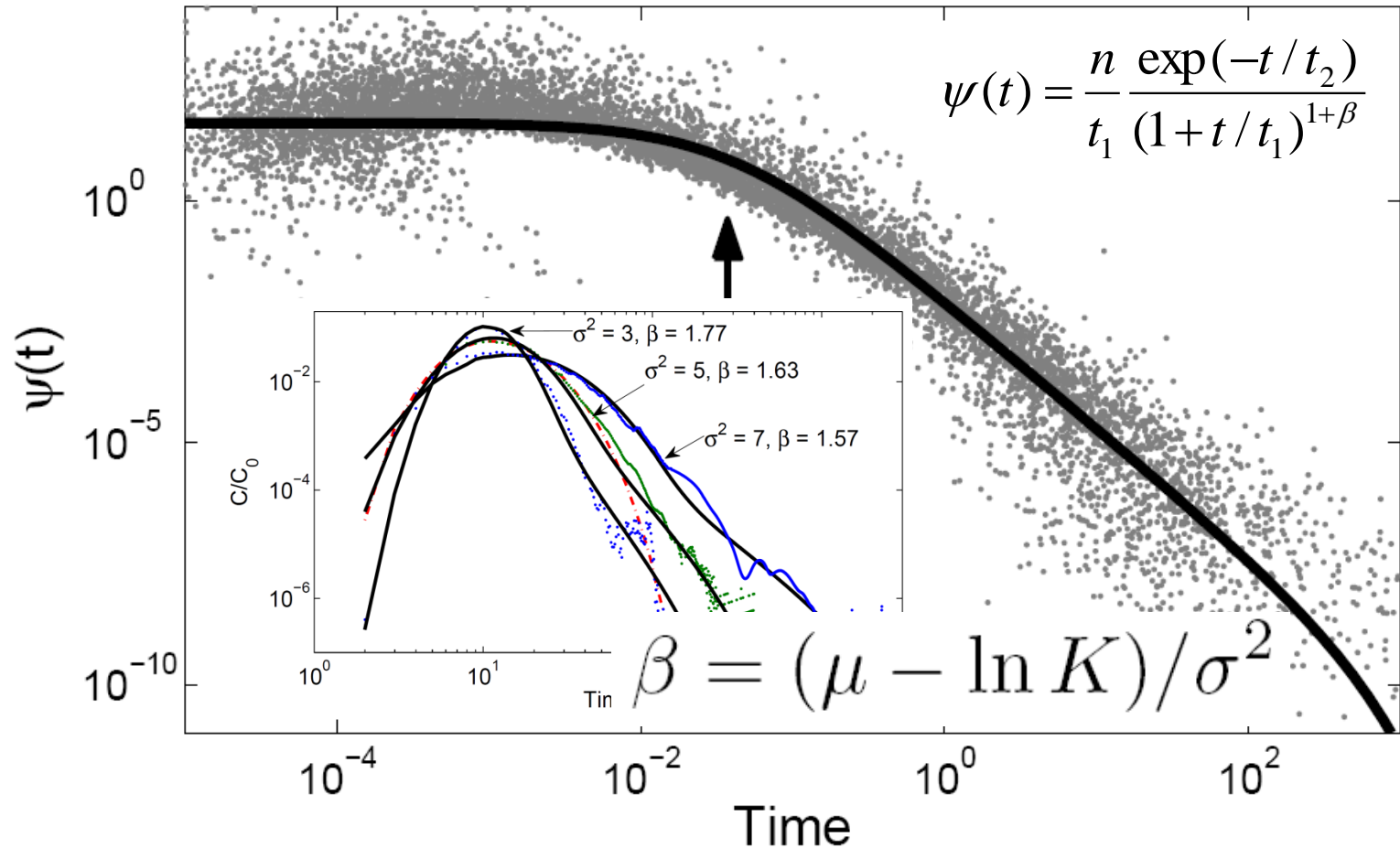


Open circles: normalized by the number of cells, for spatial map of full K field; $\sigma^2=5$; mean $\ln(K)=0.26$, skewness 0.03

Filled squares: preferential particle paths, weighted and normalized by number of particles visiting in each cell, $\{wK\}$; weighted mean $\ln(K)=1.43$, skewness 3.89

Bars in red indicate frequency of LCTs.

Natural Heterogeneity – CTRW Transport Description



Ensemble particle-weighted conductivity histogram ($\sigma^2=5$, 100 realizations); based on conductivity histogram, transforming to particle transition time distribution within cells, representing $\psi(t)$ vs. t . Solid curve shows the TPL with same values for breakthrough curve shown in inset. Arrow marks t_1 , the onset of the power law region at $t_1 < t < t_2$, corresponding to $\ln(K) < -1$.

Natural Heterogeneity – Connecting Conductivity and Transport

From conductivity histogram: determine an average head gradient over each cell (weighted by relative number of visiting particles). Then determine average residence times in these cells, for each K bin, with Darcy's law:

$$\Delta t = \theta(\Delta x)^2 / (K \Delta h)$$

⇒ obtain a frequency (weighted by relative number of visiting particles) of particle residence times in all domain cells

RESULT: statistical analysis of particle paths, which renders, the weighted K distribution (previous slide), leads directly to the CTRW $\psi(t)$!!

Functional form of weighted time distribution:

$$f = n_k \exp[-(\ln K - \mu)^2 / (2\sigma^2)] / t$$

Equate log derivative to that of TPL to develop an analytical expression for β in terms of the weighted K histogram parameters:

$$\beta = (\mu - \ln K) / \sigma^2$$

Conclusions

- “Origin” of anomalous transport: we develop a direct connection between CTRW parameters and the randomly heterogeneous hydraulic conductivity field.
- Transport cannot be explained solely by the structural knowledge of the disordered medium; dynamic/flow controls are critical factors. Low conductivity transition zones largely determine the preferential flow paths.
- A basic determinant of the distribution of local transition times, which defines the transition time pdf used in the CTRW description, is a conductivity histogram weighted by the particle flux. Agreement between simulations, pdf parameters, and matches to BTCs is convincing.
- A quantitative relationship between the power law exponent β and the statistics of the underlying (correlated) hydraulic conductivity field has been determined.
- Models based on critical path analysis and percolation theory are not applicable: the power law region of the transition times that controls the anomalous transport behavior lies below the critical path threshold.
- Use of advection-dispersion equation: particle plume convergence to this model is not due to “homogenization” of the plume sampling in the domain, but rather to focusing of flow in a limited number of relatively uniform preferential pathways.